

ESM 219

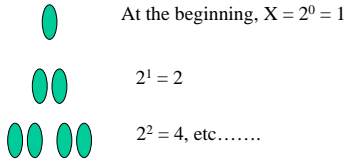
Lecture 4: Growth and Kinetics

Concepts

- Concerned with populations of cells and population numbers and characteristics
- Various ways to report population sizes
- Unrestricted cellular division is well-understood
- Mass transfer-limited growth models, including on solid media, involve more terms

Unrestricted Cell division = population growth

X = number of cells
 n = number of division events (doublings)
 $X = 2^n$



Population growth, $X = 2^n$ (cont.)

Let $n = (\# \text{ doublings / time}) * t$
 $= \text{growth rate constant} * t$
 $= \mu * t$

where $\mu = \text{“specific growth rate”}$
 Notice that equation is exponential,
 so can express as $X = e^{\mu t}$

Note that starting concentration is not 1,
 So $X = X_0 e^{\mu t}$ where X_0 is the initial concentration.

Unrestricted cell division is a “first order” rate process

- Unrestricted cell division is a first order rate process.

$$\frac{d}{dt}(X) = \frac{d}{dt}(X_0 e^{\mu t})$$

So,

$$\frac{dX}{dt} = \mu X$$

$$\frac{dX}{dt} = \mu X \quad \text{Now let's go the other direction.....}$$

$$\frac{dX}{X} = \mu dt \quad \leftarrow \text{Separate variables.}$$

$$\int_{t=0}^{t=t} \frac{dX}{X} = \mu \int_{t=0}^{t=t} dt \quad \leftarrow \text{Integrate over the interval 0 to t.}$$

$$\ln \frac{X_t}{X_0} = \mu t \quad \leftarrow \text{The result is a straight line equation.....}$$

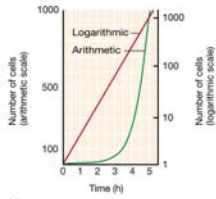
$$\ln X = \ln X_0 + \mu t$$

$$X_t = X_0 e^{\mu t}$$

And if we raised e to both sides, we'd be back where we started...

Time (h)	Total number of cells	Time (h)	Total number of cells
0	1	4	256
0.5	2	4.5	512
1	4	5	1,024
1.5	8	5.5	2,048
2	16	6	4,096
2.5	32	-	-
3	64	-	-
3.5	128	10	1,048,576

(a)



(b)

During exponential phase growth, a log-linear plot produces a straight line, because

$$\ln(X) = \ln(X_0) + \mu t$$

Microbial Laboratory Culture

Well-mixed liquid
(flask or culture tube or chemostat)

Solid media culture
(agar or sand culture)

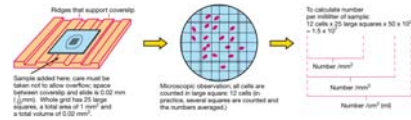


In all cases

- Prepare media with nutrients, and establish conditions required for growth
- Inoculate
 - With a small amount of known cells for pure culture
 - With an environmental sample for enrichment culture
- Monitor over time
 - Quantify population size at various time points
 - Or measure / observe beginning and end.

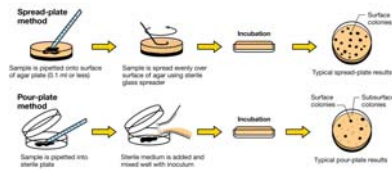
How to measure cell concentration

1. Direct counts with a microscope

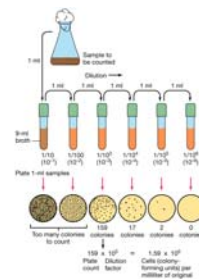


How to measure cell concentration

2. Culturable counts



With or without a dilution series.



How to measure cell concentrations

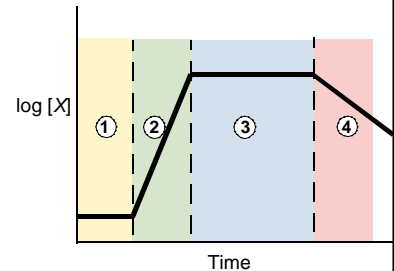
3. Flow cytometry

-----one might also measure proxies for biomass-----

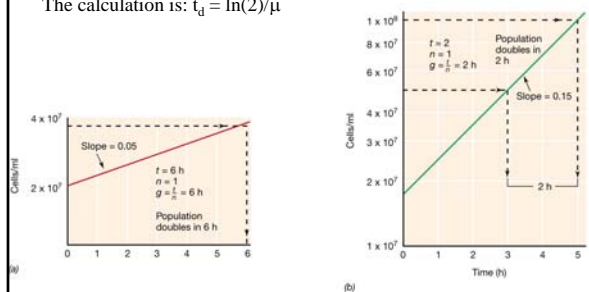
- Biochemically (DNA, protein, etc.)
- Absorbance, reported as optical density or OD (indirect based on turbidity)

Microbial Growth phases in well mixed liquid culture

- **Region 1: Lag phase**
 - microbes are adjusting to the new substrate (food source)
- **Region 2 Exponential growth phase.**
 - microbes have acclimated to the conditions
- **Region 3 Stationary phase.**
 - limiting substrate or electron acceptor limits the growth rate
- **Region 4 Decay phase.**
 - substrate supply has been exhausted



Generation time, a.k.a. doubling time, is the time required for the population to double.
The calculation is: $t_d = \ln(2)/\mu$



Exponential Phase Growth

- Log phase growth is first order, ie
- Growth rate \propto to population size
- So $\ln X$ vs. t is linear, slope = μ
- μ units are $1/t$ (i.e. hr^{-1})

$$\frac{dX}{dt} = \mu X$$

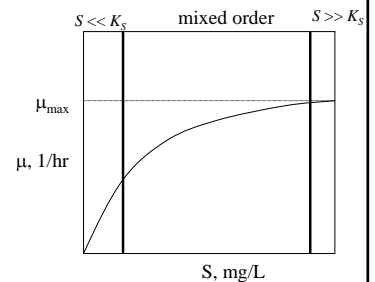
Monod Growth Kinetics

- Relates specific growth rate, μ , to substrate concentration
- Empirical---no theoretical basis---it just "fits"!
- Have to determine μ_{max} and K_s in the lab
- Each μ is determined for a different starting S

$$\mu = \frac{\mu_{max} S}{K_s + S}$$

Monod Growth Kinetics

- First-order region, $S \ll K_s$, the equation can be approximated as $\mu = \mu_{max} S/K_s$
- Center region, Monod "mixed order" kinetics must be used
- Zero-order region, $S \gg K_s$, the equation can be approximated by $\mu = \mu_{max}$



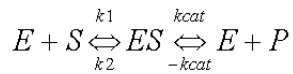
Determining Monod parameters

- Double reciprocal plot (Lineweaver Burke)
 - Commonly used
 - Caution that data spread are often insufficient
- Other linearization (Eadie Hofstee)
 - Less used, better data spread
- Non-linear curve fitting
 - More computationally intensive
- Progress-curve analysis (for substrate depletion)
 - Less lab work (1 curve), more uncertainty

Michaelis Menten Kinetics

- Used when microbe population is constant = non-growing (or short time spans)
- Derivable from first principles (enzyme-substrate binding rates and equilibria expressions)
- Parameter determination methods used for Monod calculations (i.e. Lineweaver Burke)

Michaelis-Menten Equation for Enzyme Kinetics



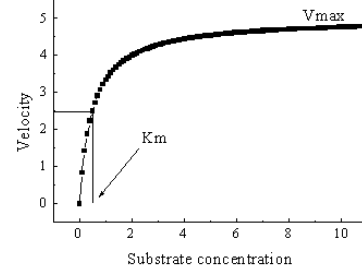
Assumptions:

1. Formation of ES complex
2. k_1 and $k_2 \gg k_{cat}$ $K_m = k_2/k_1 = [E][S]/[ES]$
3. $[S] \gg [E]$ such that $[ES]$ formation does not change $[S]$
4. $[P]$ is very small, valid for initial rates only

$$v/V_{max} = [S]/(K_m + [S]) \quad \text{Michaelis-Menten Equation}$$

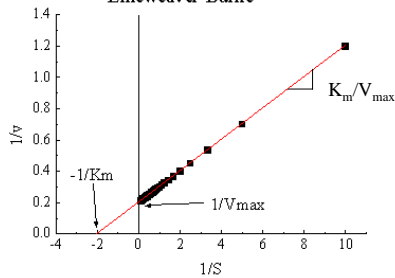
$$v/V_{max} = [S]/(K_m + [S])$$

Michaelis-Menten



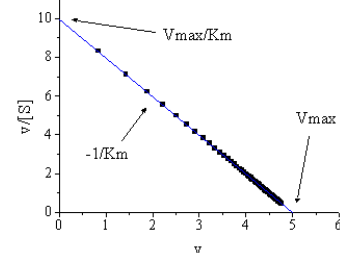
$$1/v = (K_m/V_{max})(1/[S]) + 1/V_{max}$$

Lineweaver-Burke



$$v/[S] = v(-1/K_m) + V_{max}/K_m$$

Eadie-Hofstee



Monod vs. Michaelis-Menten: recap of differences

- | | |
|---|--|
| <ul style="list-style-type: none"> • Monod <ul style="list-style-type: none"> – Growth – Empirical – K_s – μ, 1/t | <ul style="list-style-type: none"> • Michaelis Menten <ul style="list-style-type: none"> – No growth; constant E – Derived from theory – K_m – v, mg/L-t |
|---|--|

Similarities are shape of curves, form of function, parameter estimation techniques.

Substrate Depletion Kinetics

- The rate of biodegradation or biotransformation is a focus of environmental studies
- Substrate consumption rates have often been described using 'Monod kinetics'

$$-\frac{dS}{dt} = \frac{kSX}{K_s + S}$$

- S is the substrate concentration [mg/L]
- X is the biomass concentration [mg/L]
- k is the maximum substrate utilization rate [sec^{-1}]
- K_s is the half-saturation coefficient [mg/L]

Substrate Depletion Kinetics

- Since $\frac{dX}{dt} = \mu X = -Y \frac{dS}{dt}$
- And $\mu = \frac{\mu_{\max} S}{K_s + S}$
- Then $-\frac{dS}{dt} = \frac{\mu X}{Y} = \frac{\mu_{\max} SX}{(K_s + S)Y}$
- And $-\frac{dS}{dt} = \frac{kSX}{K_s + S}$ Where $k = \frac{\mu_{\max}}{Y}$

Modeling Substrate Depletion

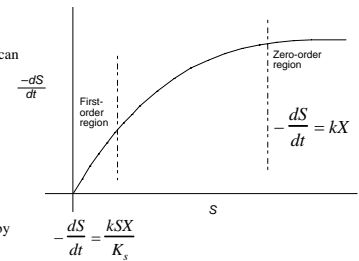
- Three main methods for modeling
 - Monod kinetics (mid range concentrations)
 - First-order decay (low concentration of S , applicable to many natural systems)
 - Zero-order decay (substrate saturated)

Modeling First-Order Decay

- $dS/dt = kS$ where k is a pseudo first order constant Generally assumes nothing about limiting substrates or electron acceptors
- Degradation rate is proportional to the concentration
- Generally used as a fitting parameter, encompassing a number of uncertain parameters

Monod Kinetics

- First-order region, $S \ll K_s$, the equation can be approximated by exponential decay ($C = C_0 e^{-kt}$)
- Center region, Monod kinetics must be used
- Zero-order region, $S \gg K_s$, the equation can be approximated by linear decay ($C = C_0 - kt$)

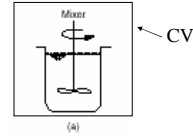


Microbial Kinetics in Modeling Fate of a Substrate

- Use mass balance framework for modeling fate of substance, S
- Choose appropriate “ideal” reactor analogy (usually batch or complete mix)
- Substitute appropriate reaction expression into the framework

Mass Balance: Batch example

- Closed
- Well-mixed
- Constant volume



Verbal: In – Out + Reaction = Accumulation

$$\text{Math: } 0 \quad 0 \quad rV \Delta t \quad \Delta S V$$

$$\text{Units: } \quad \quad \quad \text{m}^3/\text{t} \cdot \text{t} \quad \quad \quad \text{m}^3 \cdot \text{t}^{-1}$$

$$\text{Rearrange: } \quad \quad \quad r V = \Delta S / \Delta t$$

Mass Balance: Batch example

Take limits as ΔS and $\Delta t \rightarrow 0$ $r = \frac{dC}{dt}$

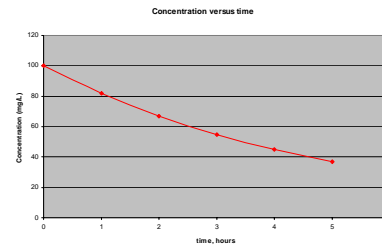
Substitute a rate equation for “r”
e.g. 1st order decay of S: $-kS$

$$S_0 \cdot -kS = \frac{dS}{dt} \quad \text{Rearrange, integrate: } \int_{S_0}^{S_t} \frac{dS}{S} = -k \int_0^t dt$$

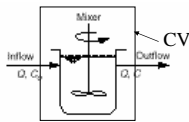
$$\int_{S_0}^{S_t} \ln S = -kt \rightarrow \frac{S_t}{S_0} = e^{-kt} \rightarrow S_t = S_0 e^{-kt}$$

Mass Balance: Batch example of exponential decay

$$S_0 = 100 \text{ mg/L}, k = -0.2/\text{hr}$$



Mass Balance: CFSTR



Verbal: In – Out + Reaction = Accumulation

$$\text{Math: } QS_0 \Delta t - QS \Delta t + r V \Delta t = \Delta S V$$

$$\text{Units: } \text{t}^3/\text{t} \cdot \text{m}^3/\text{t} \cdot \text{t} \quad \text{m}^3/\text{t} \cdot \text{t} \cdot \text{t}^{-1} \quad \text{m}^3/\text{t} \cdot \text{t}^{-1}$$

$$\text{Rearrange: } Q/V \cdot (S_0 - S) + r = \Delta S / \Delta t$$

Mass Balance: CFSTR

Take limits as ΔS and $\Delta t \rightarrow 0$

$$Q/V \cdot (S_0 - S) + r = \frac{dS}{dt}$$

→ Substitute a rate equation for “r”

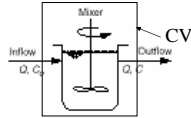
e.g. 1st order decay of S: $-kS$

→ Make *steady state* (SS) assumption (no net accumulation or depletion): $\frac{dS}{dt} = 0$

→ Rearrange

$$S = \frac{S_0}{[1 + k(V/Q)]}$$

Chemostat: CFSTR for Microbial Growth



Verbal: In - Out + Reaction = Accumulation

$$\text{Math: } QX_0 \Delta t - QX \Delta t + r V \Delta t = \Delta X V$$

$$\text{Units: } l^3/t \cdot m/l^3 \cdot t \quad m/l^3 t \cdot t \cdot l^3 \quad m/l^3 \cdot l^3$$

$$\text{Rearrange: } Q/V \cdot (X_0 - X) + r = \Delta X / \Delta t$$

Chemostat: CFSTR for Microbial Growth

Take limits as ΔX and $\Delta t \rightarrow 0$

$$Q/V \cdot (X_0 - X) + r = \frac{dX}{dt}$$

→ Substitute exponential growth equation for "r"

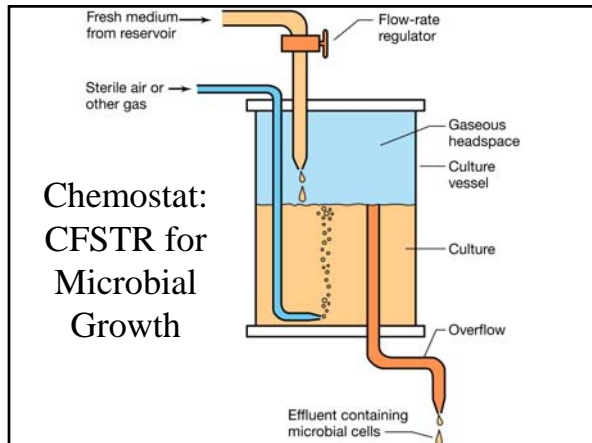
→ Set $X_0 = 0$ (no influent cells)

→ Make *steady state* (SS) assumption $\frac{dX}{dt} = 0$
(no net accumulation or depletion):

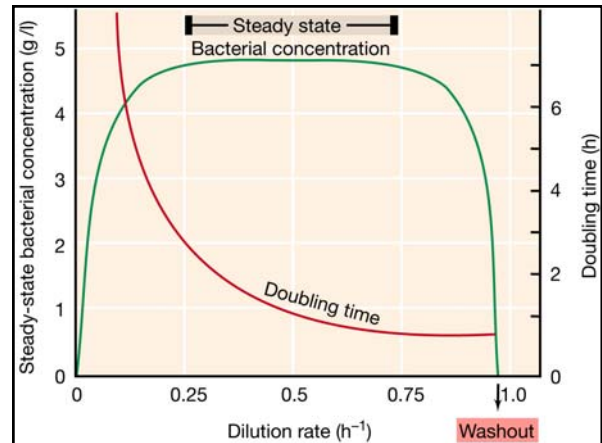
→ Let $Q/V = D = \text{dilution rate}$

→ Rearrange:

$$-\frac{Q}{V} X = \mu X \quad \rightarrow \quad -\frac{Q}{V} = \mu \quad \rightarrow \quad \boxed{D = \mu}$$



Chemostat: CFSTR for Microbial Growth



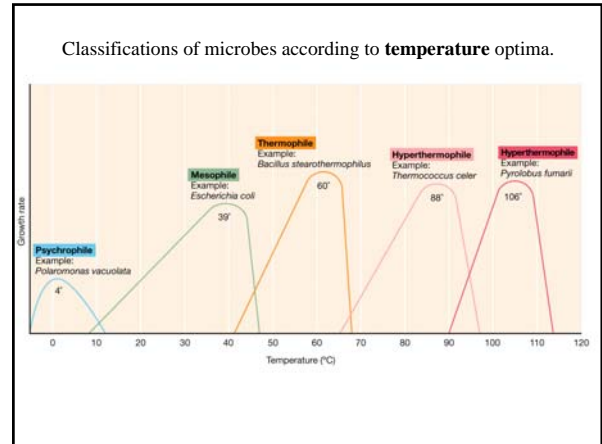
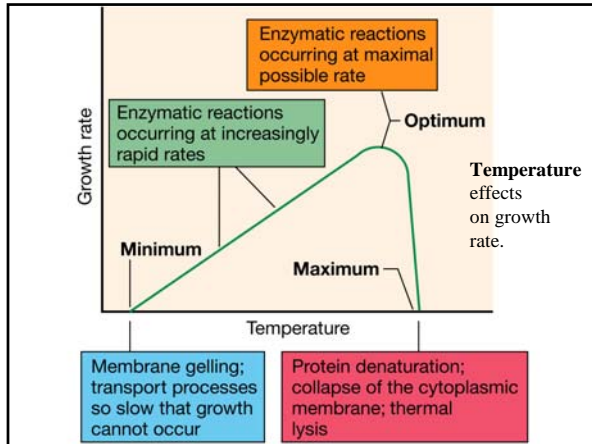
Environmental Factors

- Temperature
- pH
- Salinity
- Oxygen Concentration

Environmental Factors

Extremophiles can tolerate or perhaps require extreme conditions in any of the above.

Cellular compensation outside of their optima can reduce **growth rate** and **yield**.



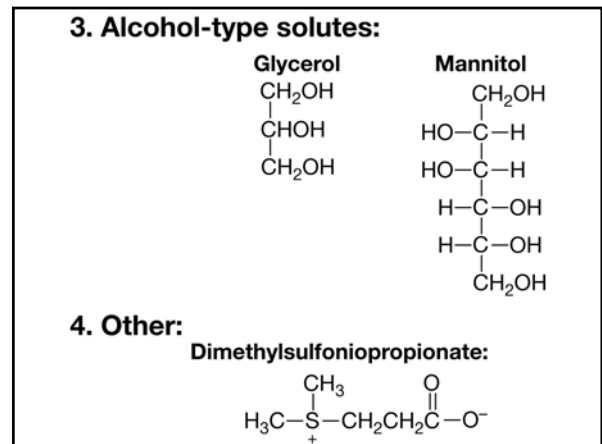
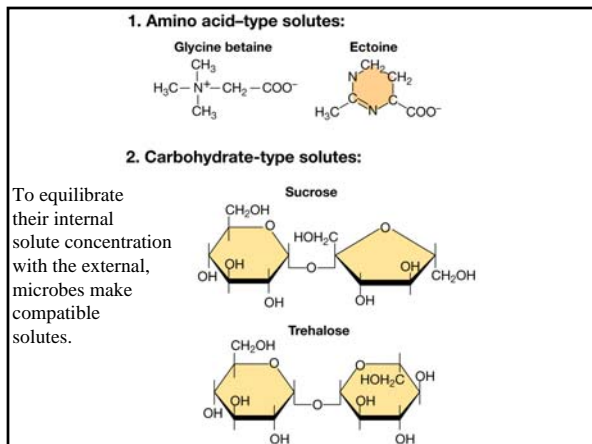
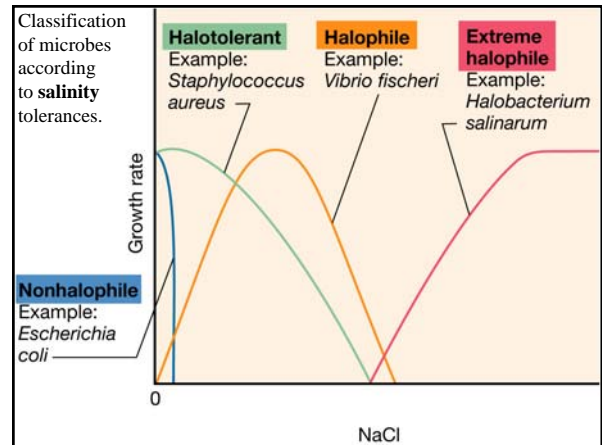
Classification of microbes according to tolerance of **pH** extremes

pH	Example	Moles per liter of: H ⁺	Moles per liter of: OH ⁻
0		1	10 ⁻¹⁴
1	Volcanic soils, waters	10 ⁻¹	10 ⁻¹³
2	Gastric fluids	10 ⁻²	10 ⁻¹²
3	Lemon juice	10 ⁻³	10 ⁻¹¹
4	Acid mine drainage	10 ⁻⁴	10 ⁻¹⁰
5	Vinegar	10 ⁻⁵	10 ⁻⁹
6	Rhubarb	10 ⁻⁶	10 ⁻⁸
7	Peaches	10 ⁻⁷	10 ⁻⁷
8	Acid soil	10 ⁻⁸	10 ⁻⁶
9	American cheese	10 ⁻⁹	10 ⁻⁵
10	Cabbage	10 ⁻¹⁰	10 ⁻⁴
11	Peas	10 ⁻¹¹	10 ⁻³
12	Corn, salmon, shrimp	10 ⁻¹²	10 ⁻²
13	Pure water	10 ⁻¹³	10 ⁻¹
14	Seawater	10 ⁻¹⁴	1

Acidophiles (Increasing acidity)

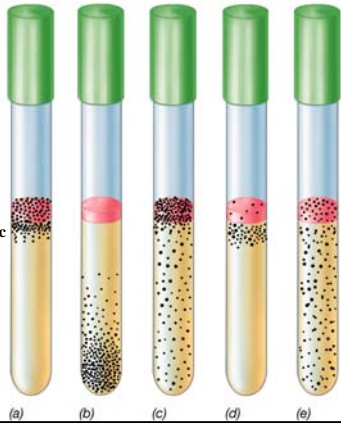
Neutrality

Alkaliphiles (Increasing alkalinity)

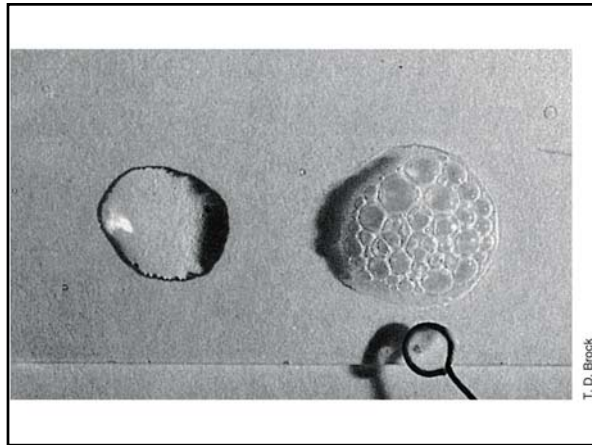
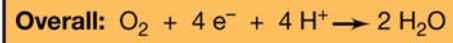
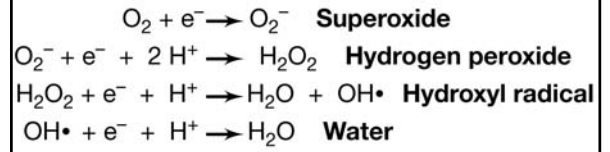


Classification of microbes according to their oxygen responses.

- a. Aerobic
- b. Anaerobic
- c. Facultative
- d. Microaerobic
- e. aerotolerant



Oxygen tolerance is conferred by enzymes that scavenge and scrub toxic free radicals. Enzymes include superoxide dismutase, catalase and peroxidase.



T. D. Brock